

# **SULFCAT**<sup>®</sup>

# Regenerative H<sub>2</sub>S Gas Scrubbing System

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### SULFCAT<sup>®</sup> H<sub>2</sub>S Removal

Hydrogen sulfide  $(H_2S)$  is a toxic and corrosive gas that occurs naturally but can also be produced through many industrial processes. In addition, H<sub>2</sub>S has an odor threshold of 0.01-0.15 ppm (OSHA). Due to the very low odour threshold, in countries where nuisance odor is regulated H<sub>2</sub>S removal from process gas or off-gas is required. Since H<sub>2</sub>S is produced through anaerobic digestion, it is prevalent where organic matter and sulfates are present. As a result, pipeline gas specifications exist to ensure natural gas quality. Furthermore, when natural gas, syngas or biogas is used in turbines or engines for power generation,  $H_2S$ concentrations cannot exceed the engine manufacturer's specifications due to corrosion concerns. Further, during combustion H<sub>2</sub>S is oxidized to sulfur dioxide, a highly regulated air pollutant which necessitates its removal before combustion. It is clear that H<sub>2</sub>S removal is important for the environment, industrial equipment integrity, and human health.

 $H_2S$  can be removed from process gas through various technologies depending on the application, process conditions and removal requirements. Some applications where  $H_2S$  treatment is of particular concern are listed below:

Landfill gas recovery

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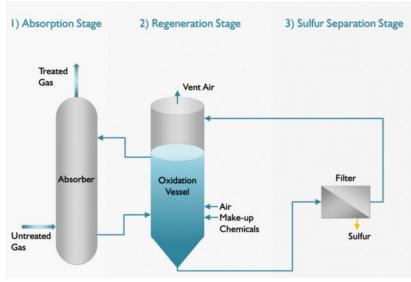
- Natural gas production
- Waste-to-energy systems,
- Biogas production, and
- Wastewater treatment plants

In all these instances,  $H_2S$  levels can range from low to high depending on the specific process conditions. For example, the recovered gas from a landfill can contain  $H_2S$  levels anywhere from a few ppm to 5% vol. This vast range is a result of the waste characteristics, more specifically, the sulfate content of the waste stream that can undergo anaerobic conversion to  $H_2S$  via sulfatereducing bacteria. As sulfate is prevalent in drywall and other construction materials, the construction and demolition (C&D) waste streams entering the landfill directly affect the levels of  $H_2S$  that will eventually be present in the landfill gas. As mentioned, various technologies are available for H<sub>2</sub>S removal, however this article will discuss the features, benefits, and application range of Macrotek's regenerative SULFCAT® technology.

#### How it Works

The SULFCAT process is a liquid redox system that works by first absorbing  $H_2S$  from the gas with a specially designed absorber tower. The  $H_2S$  then undergoes a series of reactions that convert the absorbed  $H_2S$  gas to elemental sulfur and water. The reactions are promoted by the FeRedox<sup>TM</sup> reagent that contains a suspension of stabilized, sub-micron-sized iron-based particles. The solid sulfur is filtered out of the solution and the filtrate is recycled back to the process to capture more  $H_2S$ . A number of reaction pathways occur in the process, however, all reactions can be summarized by the following overall reaction:

$$H_2S_{(g)} + \frac{1}{2}O_{2(g)} \longrightarrow S_{2(s)} + H_2O_{(l)}$$



The process contains three stages. The first is the absorption stage, where the  $H_2S$ -laden gas contacts the liquid phase, and the  $H_2S$  in the gas is selectively absorbed into the liquid. The treated gas then exits the top of the column. The  $H_2S$  removal efficiency is a function of the operating conditions and absorber design. Increasing the contact zone height and residence time increases  $H_2S$  removal efficiency. Typical efficiencies are 99.9%, but can be optimized per the process requirements.

Once the  $H_2S$  absorbs into the liquid phase, it dissociates and reacts with iron in the re-circulating liquid to form elemental sulfur and water. This reaction reduces the iron from its active oxidation state to an inactive state. The spent iron and sulfur mixture is sent to the second stage of the process, the regeneration stage. External blowers supply air to a liquid filled contactor to oxidize the iron back to its active form. The air is then vented to the atmosphere. The regenerated solution is sent back to the absorber to complete another cycle.

Finally, in the third stage, a slipstream of the liquid solution is sent to a filtration system to separate the solid sulfur from the solution. The filtrate is recycled back to the process while the low moisture content sulfur filter cake is discharged from the system.



The defining feature of the SULFCAT process is that the chemistry is regenerative, meaning the iron that is used to convert the  $H_2S$  to sulfur is continually regenerated directly within the process rather than being consumed. This results in substantially reduced chemical make-up and waste generations rates compared to non regenerative technologies.

Previously, liquid redox systems were best suited for applications with high  $H_2S$  loadings including natural gas, syngas and landfill gas applications. However, through the development of the SULFCAT process, the application range has been widened and the technology is now suitable for lower  $H_2S$  levels.

# Alternative H<sub>2</sub>S Removal Technologies

 $H_2S$  can be removed from process gas through various technologies depending on the application, process conditions and removal requirements. Most  $H_2S$  removal technologies fall under the non-regenerative classification. Examples of these technologies are chemical oxidation scrubbers, liquid or solid scavengers, and activated carbon beds. A brief description of each technology is provided below.

#### **Chemical Oxidation**

In a chemical oxidation scrubber, sodium hydroxide (NaOH) is used to neutralize  $H_2S$  after absorption into the scrubbing liquid. The absorbed  $H_2S$  is then oxidized using a chemical oxidizing agent, typically hydrogen peroxide ( $H_2O_2$ ) or sodium hypochlorite (NaOCI), to form soluble sodium sulfate (Na<sub>2</sub>SO<sub>4</sub>). Chemical oxidation scrubbers are compact and low in capital cost, however, the rate of chemical consumption and wastewater generation can be high relative to the amount of  $H_2S$  that is treated.

#### Scavengers

Scavengers can either be liquid or solid phase media that react with  $H_2S$ . Typically these reactions are irreversible (non-regenerative) resulting in the need to periodically replace and dispose the scavenger. The most common liquid scavenger are triazines which react with  $H_2S$  to form water soluble sulfur compounds. Common solid scavengers include metal oxides, particularly iron, which react with  $H_2S$  to form sulfides. Similar to chemical oxidation scrubbers, scavenger systems are relatively low in capital cost but high in operating cost due to the singleuse scavenger media.

### Activated Carbon Bed

Adsorption of  $H_2S$  is a physical process where  $H_2S$  is captured onto the surface of activated carbon. The media has a large specific surface area due to its inner pore structure that provides a large adsorptive capacity. Like scavenger systems, activated carbon is a single-use chemistry and the carbon must be manually replaced after it is fully spent.

Process Features	SULFCAT®	Chemical Oxidation	Scavengers	Activated Carbon
Minimal Waste Generation	$\checkmark$			
Regenerative Reagent	$\checkmark$			
Low Reagent Consumption	$\checkmark$			
Usable By-Prod- uct Generation	$\checkmark$			
Low Fresh Water Requirement	$\checkmark$		$\checkmark$	$\checkmark$
Low Operating Costs				
Low Capital Costs			$\checkmark$	$\checkmark$

# Comparing SULFCAT to Competing Technologies

The primary differentiator between SULFCAT and the alternative technologies discussed above is that the chemistry is regenerative. This results in substantially reduced operating costs due to the lower chemical make-up rates and waste generation rates. The difference in rates can be illustrated by the following example.

Process conditions:

- Gas Type: Landfill gas
- Gas Flow: 5000 scfm
- H<sub>2</sub>S Concentration: 2500 ppm
- Required H<sub>2</sub>S Outlet 25 ppm

In this example, a landfill is recovering and treating their gas to be sent to a gas-to-energy plant. The  $H_2S$  levels in the gas must be reduced to 25ppm to meet the engine's required inlet specifications. The landfill is considering two technologies for the treatment of  $H_2S$ : a chemical scrubber and the SULFCAT process. The following table compares the primary process inputs and outputs for each option.

	SULFCAT®	Chemical Oxidation Scrubber
Chemical Usage	11 kg/hr <sup>1</sup>	190 kg/hr <sup>2</sup>
Water Usage	80 kg/hr	200 kg/hr
Water Generation	60 kg/hr	600 kg/hr
Power	55 HP	10 HP

<sup>1</sup> FeRedox and 50% NaOH

 $^2$  50% NaOH and 50%  $H_2O_2$ 

While the power consumption is slightly higher, the chemical make-up rates and the waste generation rates for the SULFCAT option are a small fraction of those of a chemical oxidation scrubber. The operating cost is also a small fraction, representing a 90% reduction compared to a chemical oxidation scrubber.

# The SULFCAT Advantage

The SULFCAT system is of rugged construction to meet the needs of any industrial environment. The equipment is also modularized and pre-packaged to allow the shortest lead time, installation time, and lowest installation cost possible.

For applications where  $H_2S$  loading is variable and future process conditions are difficult to predict, a SULFCAT system can easily be optimized after original installation to increase the design capacity without overhauling the original equipment.

Recent advancements in instrumentation and control systems have reduced operator interaction and improved system reliability. The automated control system handles much of the day to day process variability, allowing operators to focus on other areas of the plant. Remote access to the control system also enhances an operator's ability to monitor and even make control adjustments to the system remotely.

The SULFCAT process uses non-toxic chemistry for the conversion of  $H_2S$  to solid sulfur. The near-ambient temperature and pressure also make the system inherently safe to operate.

In some cases, the sulfur that is produced in the system can be sold to sulfur producers or the agriculture industry. This potentially converts an expense to a revenue generating stream.

The SULFCAT process can be used in most applications where the  $H_2S$  loading in the gas between 0.05 to 15 tonnes per day. Since the FeRedox reagent is selective to  $H_2S$ , the CO<sub>2</sub> or other non-condensable content in the gas has minimal effect on the system, therefore a wide variety of gases can be processed from combustible gases to simply  $H_2S$ -laden air streams.





# Conclusion

The regenerative, modularized and automated nature of the SULFCAT® system results in an attractive and feasible solution for  $H_2S$  removal. Compared to non-regenerative technologies, the lower operating costs result in short payback periods and substantial long term savings.

In the past, liquid redox systems were best suited for applications with very high  $H_2S$  loadings. The high capital cost of a liquid redox system resulted in a technology which was not economically feasible for lower  $H_2S$  loadings. The SULFCAT process represents an advance in the technology which now expands the application range to moderate and even low levels of  $H_2S$ , making the SULFCAT system one of the most cost-effective methods of treating  $H_2S$  available on the market today.



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